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<b>(21) International Application Number:</b> PCT/US92/10216 <b>(22) International Filing Date:</b> 24 November 1992 (24.11.92)  <b>(30) Priority data:</b> 07/799,488                      27 November 1991 (27.11.91)    US  <b>(71) Applicant:</b> CALGON CARBON CORPORATION [US/ US]; 500 Calgon Carbon Drive, Pittsburgh, PA 15205 (US).  <b>(72) Inventors:</b> DOUGHTY, David, T. ; 364 Meade Drive, Cor- aopolis, PA 15108 (US). KNEBEL, William, J. ; 719 Sky- view Drive, Mars, PA 16046 (US). COBES, John, W., III ; 1109 Rebecca Court, Oakdale, PA 15071 (US).		<b>(74) Agent:</b> WETTACH, Thomas, C.; Reed Smith Shaw & McClay, P.O. Box 2009, Pittsburgh, PA 15230 (US).  <b>(81) Designated States:</b> CA, JP, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).  <b>Published</b> <i>With international search report.</i>
<b>(54) Title:</b> CHROMIUM-FREE IMPREGNATED ACTIVATED UNIVERSAL RESPIRATOR CARBON FOR ADSORP- TION OF TOXIC GASES AND/OR VAPORS  <b>(57) Abstract</b>  <p>Impregnated activated carbon adsorbents for the removal of toxic materials from gas streams are used in a variety of respi-          ration and collective filter applications. The impregnated activated carbon adsorbents of the present invention remain effective in          removing toxic gases and/or vapors in industrial and other applications, and are free of chromium and its potential health ha-          zards. Generally, these activated carbons are comprised of an activated carbon adsorbent impregnated so as to result in an acti-          vated carbon generally containing up to 10 % molybdenum and up to 10 % sulfate, 0 to 20 % copper, 0 to 20 % zinc, optionally          supplemented according to the desired characteristics with water or otherwise provided with moisture. Aqueous ammonia may be          used as a preparation solvent for impregnating the copper, zinc, molybdenum and/or sulfate. The universal adsorbent carbons of          the present invention have been found to be effective for removing a variety of toxic gases and/or vapors, and provide simultane-          ous protection for CEN Classification gases of Types A, B, E and K. The specific agents that the present invention removes effec-          tively includes chlorine, hydrogen chloride, hydrogen cyanide, sulfur dioxide, hydrogen sulfide, formaldehyde, carbon tetrachlo-          ride, ammonia and others.</p>		

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TITLE**CHROMIUM-FREE IMPREGNATED ACTIVATED UNIVERSAL RESPIRATOR CARBON  
FOR ADSORPTION OF TOXIC GASES AND/OR VAPORS**

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FIELD OF THE INVENTION

The present invention relates to impregnated activated carbon adsorbents for removal of toxic materials in respirator and collective filter applications and, in particular, to a universal chromium-free impregnated carbon adsorbent for the removal of toxic gases and/or vapors in industrial applications.

BACKGROUND OF THE INVENTION

Activated carbon has long been used to remove toxic gases and vapors from a stream of gas or liquid. These activated carbons are also useful in cleaning breathing air or exhaust gases by removing various noxious agents, and may be used in gas mask filters, respirators, collective filters and other applications, and often involve the use of special impregnants to remove gases that would not otherwise be removed through the use of unimpregnated, activated carbons. Prior formulations contain chromium and/or other agents impregnated on an activated carbon, and function as adsorbents effective in removing a variety of toxic materials from a vapor or liquid. In many applications, it is desirable that a single impregnated adsorbent be effective against a range of toxic agents in a gas stream.

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Known military use formulations designed to remove gases such as cyanogen chloride, hydrogen cyanide and cyanogen often contain chromium, copper, silver and other metals impregnated on an activated carbon. These  
5 adsorbents are effective in removing a large number of toxic materials. Appendix I sets forth a summary of known art involving these and other formulations.

Copper and silver have been shown to be effective in the removal of arsine and phosphine.  
10 Chlorine, hydrogen chloride, hydrogen fluoride and hydrogen sulfide are also removed by the presence of copper impregnates on activated carbon.

A number of references describe the various impregnates that may be used on activated carbon:

15 U.S. Patent No. 5,063,196 discloses copper, zinc and triethylenediamine, along with other impregnates on activated carbon for military and industrial applications. U.S. Patent Application Nos. 07/537,311 (subject to Secrecy Order) and 07/737,369, continuation-in-part  
20 applications of this patent, disclose these and other impregnates on activated carbon.

British Patent No. 2,187,725 discloses activated charcoal impregnated with transition metal salts preferably consisting of cobalt, nickel or zinc acetate.

25 U.S. Patent No. 3,355,317 to Keith et al. discloses the use of the oxides of cobalt, copper, zinc, iron and molybdenum on activated carbon to remove hydrogen cyanide from tobacco smoke.

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U.S. Patent Nos. 2,920,050 to Blacet et al. and 2,920,051 to Morse et al. describe the preparation of filters which include copper, chromium, silver and molybdenum impregnants.

5 U.S. Patent No. 4,801,311 to Tolles discloses an activated carbon filter material impregnated with copper, silver, and molybdenum and/or vanadium salts together with triethylenediamine.

10 U.S. Patent No. 4,802,898 to Tolles discloses an activated carbon filter material impregnated with triethylenediamine, and optionally with copper and silver.

U.S. Patent No. 4,531,953 to Groose discloses an activated carbon impregnated with copper, silver and/or chromium mixtures and triethylenediamine.

15 U.S. Patent No. 4,677,096 to van der Smisen discloses an activated carbon, silica gel, molecular sieves or activated alumina which contains zinc oxide with other impregnates.

20 U.S. Patent No. 4,636,485 to van der Smisen discloses catalysts and other impregnates on porous substrates to include activated carbon.

These and other references, including the 1946 NDRC report (Appendix I, Reference 10) by Grabenstetter et al. describe the use of chromium, copper, silver, 25 molybdenum, vanadium and other impregnants on activated carbon.

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The use of impregnated activated carbon adsorbents in respirators and collective filters, either for military or industrial applications, require special considerations regarding the toxicity and carcinogenicity of the impregnants to the user. These considerations eliminate a large number of prior art potential impregnants from use in respirator and collective filter applications. This is especially the case with hexavalent chromium; for example, the wearer of a protective mask which employs a filter containing hexavalent chromium may suffer adverse consequences due to exposure to this potential health hazard.

Known formulations include a variety of materials impregnated in activated carbon to remove toxic vapors from a gas stream. The industrial requirements for the removal of such gases is described in European Standard; Respiratory Protective Devices: Gas Filters and Combined Filters: Requirements, Testing, Marking; Document CEN/TC 79/SG4-186E; pr EN141; October 1987.

German Standard DIN No. 3181 has established standards for protection against various noxious substances. As an example, breathing filters are to be marked with the identification letter "A" when they protect against organic vapors, with letter "B" when they protect against acid gases such as HCN, H<sub>2</sub>S and Cl<sub>2</sub>, with letter "E" when they protect against SO<sub>2</sub>, and with letter "K" when they protect against NH<sub>3</sub>. A filter that protects against all such Type A, B, E and K toxic agents may appropriately be marked "A-B-E-K".

Non-impregnated activated carbons are generally effective against Type A toxic agents. Over the years, a number of filters have been developed so as to be suitable for removing gases of Type A, B, E and K, as well as combinations thereof. Metals and metal oxides of the

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first-row transition metal series, such as chromium and copper, are often indicated as the impregnating agents. In preparation of the filter media, the carbon is first treated with a metal reagent, and then the freshly  
5 impregnated mixture is dried and heat treated to deposit and to decompose the metal compound to its oxide. This impregnated carbon, while useful for Types A, B and/or E, depending on the application, may not be suitable as an air purification agent for other applications and/or for  
10 filters requiring a wider range of utility.

Applications requiring filters that protect against a mixture of Types B or E and K toxic agents require filter media which protect against acid gases and alkaline species such as ammonia gases. For example,  
15 combined protection against Types A, B and K toxic agents has previously been attained by impregnating a first filter media with a preparation effective against acid gases and by impregnating a second filter media with a preparation effective against alkaline species such as  
20 ammonia. These filter media are thereafter assembled in series into a two-stage filter in a single container, so as to be effective against Types B and K toxic agents (as well as against Type A toxic agents, which only require activated carbon as the filter media).

25 The shortcomings of two-stage filters are easily understood; they are bulkier, require more space, and are heavier than single stage filters. As minimum fill volumes of each stage must be used to meet the required performance parameters, the carbon bed dimensions  
30 (including depth or length) must be sufficient so as to allow proper contact or residence of the agent. As such, two-stage filters may not simply be made smaller or thinner so as to be advantageous to the user. Likewise, such two-stage filters result in increased flow resistance  
35 to gases through the entire filter. This effect can be debilitating to a respirator wearer who during an emergency (or routine situation involving manual labor) must breathe through a respirator that causes such a flow resistance.

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Furthermore, any added resistance to the flow of inhaled air can be expected to have a negative effect on the proper "seal" of an individual respirator mask against the face of its wearer. A mask that includes a filter with greater resistance to inhalation by the user increases the likelihood that this seal may be broken, permitting poisonous gases to reach the lungs of the mask-wearer. An effective single-stage filter will consume less space, which in many situations requiring operations in close quarters, may prove to provide significant advantages over more bulky protective filters.

Similarly, the disadvantages of bulkiness and increased airflow resistance are likewise present in collective protection systems when multiple filters are used. In contrast, the reduced flow resistance to gases through single-stage filters permit a smaller, more efficient air pump to be used, which may prolong the operating life of the pump under such reduced operating pressures. Further, the reduced resistance to flow that can be achieved with a single-stage collective protection filter can be expected to permit a tighter, more reliable seal due to the lower operation pressures associated with such filters.

Likewise, admixtures of carbons impregnated according to preparations effective against different gases are known, and are also subject to the difficulty of attaining uniform blending. They would also suffer many of the disadvantages of bulkiness and pressure drop associated with multiple-stage filters.

Accordingly, the present invention is intended to provide a "universal" filter containing impregnated activated carbon that is effective in removing Type A, B, E and K toxic agents from gases and/or vapors, and may be used in industrial respirator, collective filter, and other applications. The impregnates used for the universal carbon (or other substrate) of the present invention may be impregnated on activated carbon in an efficient, reliable and cost-effective manner.



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The present invention is able to provide an activated carbon that has the advantages of a chromium-free adsorbent while retaining its effectiveness in removing toxic gases and/or vapors. The single  
5 "universal" filter of the present invention containing said impregnated activated carbon is effective in removing Types A, B, E and K toxic agents from gases and/or vapors, yet avoids the health hazards associated with chromium-containing adsorbents.

10 The present invention is also able to provide for a more compact and easy-to-use individual, collective or similar filter. The universal carbon of the present invention is effective in smaller bed sizes, so as to permit lowered resistance to the flow of gases through  
15 that filter. When protection for all types of agents is not required, or in applications when shorter breakthrough periods are permitted, the impregnants and substrate may be modified so as to be effective in a particular desired application.

20

#### SUMMARY OF THE INVENTION

The present invention generally comprises a porous substrate onto which has been deposited various metal compounds (i.e., copper, zinc and molybdenum in the forms of carbonates, oxides and sulfates) which are  
25 capable of sorption of a number of toxic gases as contaminants in various air mixtures.

The substrate may be impregnated so as to contain, in combination, zinc carbonate (or oxide), copper carbonate (or oxide), zinc (or copper) sulfate and a  
30 molybdenum (VI) oxide moiety. The resulting homogeneous composite media can be adapted to give

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balanced properties which simultaneously satisfy the filter requirements containing Types A, B, E and K gases. Importantly, the chromium-free universal carbons of the present invention possess desirable sorptive capacities and service lives for each toxic agent, and can be manufactured and implemented as a single-stage filter media for multi-range protection.

Embodiments of the present invention have been found to be effective for removing, neutralizing and/or scavenging various toxic agents including, but not limited to, HCN, H<sub>2</sub>S, Cl<sub>2</sub>, SO<sub>2</sub> and NH<sub>3</sub>, as well as for providing the desired capacity for the physisorption of organic vapors including that of CCl<sub>4</sub>.

Within this media, the components of zinc carbonate (or oxide) and copper carbonate (or oxide), alone and in combinations thereof, serve primarily to remove or effectively isolate acid gas species. Sulfates of zinc or copper are used as impregnates or are formed in situ so as to substantially enhance the ability of the media to adsorb ammonia. The addition of sulfates provides adsorption capacity beyond that provided by the zinc carbonate (or oxide) and copper carbonate (or oxide) matrix which, by itself, contributes minimally toward the latter sorptive process. The addition of the above impregnants to the substrate is accomplished in such a manner that they do not prohibitively limit the physical adsorption capacities toward organic vapors.

By selecting a suitable mixture with all the aforementioned constituents and appropriate conditions for the impregnation, drying and heat-treatment processes, an activated carbon can be impregnated in such a manner acceptable for the manufacture of a multi-range filter media which can provide protection for both acid and base gases. Thus, a combination of zinc and/or copper

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carbonates or oxides, zinc and/or copper sulfates or zinc and copper with sulfate, and molybdenum or its oxide can provide effective universal chromium-free filtering of Types A, B, E and K agents.

5           The universal respirator carbon of the present invention meets all CEN Standards to Types A, B, E and K for Class 2 industrial filter applications, as set forth in Table I. This objective can notably be met utilizing fill volumes of 300 ml or less, which can outperform  
10 competitive filters that do not possess the advantages of the chromium-free universal filters of the present invention.

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Table I

15           CEN Requirements for Class 2 Respirator Protection.

<u>Gas</u>	<u>Type</u>	<u>Inlet Concentration (ppm)</u>	<u>Outlet Concentration (ppm)</u>	<u>Service Life (min)</u>
CCl <sub>4</sub>	A	5000	10	40
20 Cl <sub>2</sub>	B	5000	0.5	20
H <sub>2</sub> S	B	5000	10	40
HCN	B	5000	10	25
SO <sub>2</sub>	E	5000	5	20
NH <sub>3</sub>	K	5000	25	40

25 -----

The present invention is effective in a broad range of compositions, to include porous activated carbon adsorbents impregnated to provide a final composition containing (each by weight percent) up to 20% or more zinc  
30 (as ZnCO<sub>3</sub>, ZnSO<sub>4</sub>, ZnO or ZnMoO<sub>4</sub> equivalents), up to 20% or more copper (as CuCO<sub>3</sub>, CuSO<sub>4</sub>, CuO or CuMoO<sub>4</sub> equivalents),

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up to 10% or more  $\text{SO}_4^{2-}$  (directly or as copper or zinc sulfate), up to 10% or more molybdenum (as  $\text{Mo}_2\text{O}_7^{2-}$  or  $\text{MoO}_4^{2-}$  equivalents) and up to 25% water or moisture. These formulations may be varied, depending on the particular application and/or performance characteristics desired. The addition of triethylenediamine (TEDA) would provide cyanogen chloride protection, although a composition that includes TEDA may not perform as would other universal carbons. Those familiar with the art of adsorption by impregnated carbons will recognize that the positive effects of the carbons of the present invention are to an extent only limited by the theoretical impregnation limits of the materials used and the particular balance of performance attributes desired.

Preferred embodiments of the present invention comprise an activated carbon adsorbent impregnated so as to result in a composition containing, by weight, from about 0-8% zinc (as  $\text{ZnCO}_3$  or  $\text{ZnO}$  equivalents), 6-10% copper (as  $\text{CuCO}_3$  or  $\text{CuO}$  equivalents), 6-10% zinc and copper (as  $\text{ZnCO}_3$ ,  $\text{ZnO}$ ,  $\text{CuCO}_3$  or  $\text{CuO}$  equivalents), 2-4% (w/w) zinc/or and copper (as  $\text{ZnSO}_4$  or  $\text{CuSO}_4$  equivalents), 1-4% (w/w) molybdenum (as  $\text{Mo}_2\text{O}_7^{2-}$  or  $\text{MoO}_4^{2-}$  equivalents) and 5-10% (w/w) water or moisture. These impregnants can be effectively dispersed over a coal-base granular (12x30 mesh) activated carbon, or similar porous media.

A specific preferred embodiment of the present invention also may include formulations comprising activated carbon impregnated with about 11% copper, 3.5% sulfate, 2.0% molybdenum and 5.0-7.0% water impregnated into activated carbon. This embodiment performs up to approximately 20% better than CEN specifications at a fill volume of 300 ml and 35% better at a fill volume of 350 ml. This universal carbon exceeds the performance of the best competitive materials, and will at the same time provide substantial protection against formaldehyde, hydrogen chloride and others.

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As such, the universal filters of the present invention have wide-ranging utility, give balanced performance, and exceed the test standards as defined in the CEN Standards Methodology for Europe. The filters of the present invention also meet certain NIOSH standards. The sorptive media of the present invention, when incorporated into a respirator cartridge or canister unit associated with a respirator gas mask, collective protection device or similar application, is effective toward the generation of a purified effluent of acceptable qualities for breathing or other use in an industrial environment without the hazards associated with chromium-impregnated carbons.

#### PRESENTLY PREFERRED EMBODIMENTS

##### 15 Overview of Tests Conducted

A number of evaluations were designed and conducted to evaluate A-B-E-K performance of the carbons of the present invention. Evaluations of the protection provided against the challenges of the agents  $\text{NH}_3$ ,  $\text{SO}_2$  and  $\text{CCl}_4$  were initially measured, as it had been determined that performance against these agents would be more critical in the design of a new universal chromium-free industrial carbon. The A-B-E-K agent sorption properties were tested on various carbon formulations at several media bed depths, aimed at maximizing overall performance of the universal carbons being evaluated. A variety of base carbons were tested, to include impregnated activated coal-based 12x30 mesh carbon, 12x20 mesh carbon, as well as other granular and pelletized coal and wood-based carbons. Several methods were evaluated to determine the most effective method of integrating the various required adsorptive properties.

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The comparative breakthrough tests included evaluations of other universal canisters (Class 2 Industrial Filters), which were observed to have fill volumes of approximately 300-320 ml for Type A2B2E2K1 and approximately 350-380 ml for Type A2B2E2K2 filters. The media bed depth ranged from approximately 35-47 mm within canisters of diameters generally ranging from 100-105 mm. Pelletized commercial chromium-containing carbons having a pellet size of 0.8-1.2 mm and granular materials with a particle size range of approximately 12x30 mesh were tested as universal filter media. All tested media contained copper (approximately 3-7 wt.%) and chromium (approximately 1-3 wt.); in addition, some contained zinc in a range of about 2-8 wt.%. All carbons contained various levels of moisture generally ranging from approximately 7-13 wt.%. The commercially available media appeared homogeneous in composition throughout the bed depth of the filter. Many such chromium-containing materials are capable of meeting or exceeding the CEN concentration/service life standards for Types A, B, E and K agents.

Tests were performed on several of these chromium-containing products available in the U.S. and/or European marketplace utilizing 350 ml fill volumes, as shown in Table II below. The products tested in Table II included carbons impregnated with chromium and other materials.

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Table II

## AVAILABLE CHROMIUM-CONTAINING PRODUCTS

Service Life (min.) for 350 ml fill volume.

5	<u>Carbon</u>	<u>NH<sub>3</sub></u>	<u>SO<sub>2</sub></u>	<u>CCl<sub>4</sub></u>	<u>H<sub>2</sub>S</u>	<u>HCN</u>	<u>Cl<sub>2</sub></u>
	Sample A	40	29	42	---	65	46
	Sample B	17	25	42	---	28	---
	Sample C	35	24	55	101	42	22
	Sample D	46	27	41	---	56	25
10	-----						

Preparation and Evaluation of Formulations

15 The variables which can affect the performance of the universal carbon product include: (1) the particular impregnants to be used, the level of these impregnants, and the initial compound from which these impregnants are obtained; (2) the solvent used to dissolve the impregnating compounds; (3) the method of impregnating the carbon base material; (4) the procedure used to dry the impregnated carbon; (5) the amount of moisture present or added; and (6) the base carbon to be impregnated and the activity of this carbon.

25 In order to explore the effect of these variables, a series of samples was prepared and tested. Test studies were conducted using various combinations of zinc carbonate, copper carbonate, zinc sulfate and/or copper sulfate added to an ammoniacal solution with a constant amount of ammonium dimolybdate.

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A typical impregnation solution for a test sample (Sample #16 in Table III) is as follows:

	<u>Quantity</u>	<u>Material</u>
	560 ml	H <sub>2</sub> O
5	255 g	(NH <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>
	317 ml	NH <sub>4</sub> OH
	139 g	ZnO
	68 g	CuCO <sub>3</sub> Cu(OH) <sub>2</sub>
	22 g	(NH <sub>4</sub> ) <sub>2</sub> Mo <sub>2</sub> O <sub>7</sub>
10	1000 g	12 x 30 mesh granular carbon

Aqueous ammonia was the solvent used to dissolve the initial metal compounds for impregnation on activated carbon. The addition-titration method was used to impregnate the carbons, in which the desired solution was added slowly with mixing to the carbon, almost to the point of wetness. One or more impregnation "cycles" may be used. For the two-cycle impregnations, the first cycle included the addition of approximately 175 ml of solution per 250 grams of carbon, and the second cycle included adding approximately 125 ml solution per 250 grams of carbon. Drying between the two impregnations was performed. Other methods of impregnation, to include dunking and spraying, should also be acceptable.

Drying of the samples in Table III below was accomplished via temperature "ramping", as follows: (1) First impregnation a) 100°C for 30 min.; and b) 130°C for 30 min.; (2) Second impregnation a) 100°C for 30 min.; b) 130°C for 30 min.; c) 160°C for 45 min.; and d) 180°C for 45 min.

After drying, samples were moisturized to the indicated levels by adding water. As such, the weight percent of H<sub>2</sub>O in all Tables herein is based on final wet product weight. The weight percent of all other impregnates is relative to the final dry weight of the impregnated activated carbon. A variety of moisture/water addition methods, such as exposing the carbon to a humid stream of air, should also be acceptable.



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Table III sets forth the performance of a number of the chromium-free universal carbon formulations of the present invention.

Table III

5                      Universal Carbon Formulation Tests

	Sample #	Impregnants (by wt. percent)					Bed Depth (mm)	Service Life (min)		
		Zn	Cu	Mo	SO <sub>4</sub> <sup>2-</sup>	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
10	1	9	2.5	1	4.3	6	35 40	39 46	21 24	48 --
	2	8.5	3	1	4.3	6	35 40	38 49	21 23	49 54
15	3	8.5	3	1	4.3	6	35 40	42 45	21 26	49 --
	4	8.5	3	1	4.3	6	35 40	45 49	24 26	51 60
20	5	8.5	3	1	4.3	6	35 40	38 40	24 26	46 --
	6	8.5	3	1	4.3	6	35 40	43 45	23 28	43 52
	7	8.5	3	1	2.2	6	35 40	31 35	29 34	42 52
25	8 <sup>1</sup>	8.5	3	1	4.3	6	35 40	29 --	24 27	48 --
	9 <sup>1</sup>	9	2.5	1	4.3	6	35 40	28 --	24 29	46 --
30	10	3	8.5	1	4.3	6	35 40	41 46	25 29	47 --
	11	12.5	--	--	4.3	6	35 40	30 37	22 25	51 --

<sup>1</sup> 1% Na added.

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Table III (Continued)

## Universal Carbon Formulation Tests

5	Sample #	Impregnants (by wt. percent)					Bed Depth (mm)	Service Life (min)		
		Zn	Cu	Mo	SO <sub>4</sub> <sup>2-</sup>	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
	12 <sup>2</sup>	8.5	3	1	4.3	6	35 40	38 48	21 26	45 --
	13 <sup>3</sup>	3	8.5	1	4.3	6	35 40	41 49	26 29	48 --
	14 <sup>3</sup>	11.5	--	1	4.3	6	35 40	38 45	25 27	49 --
	15 <sup>2,3</sup>	8.5	3	1	4.3	6	35 40	26 --	26 28	45 --
	16 <sup>3</sup>	8.5	3	1	4.3	6	35 40	42 47	23 --	44 --
	17 <sup>3</sup>	8.5	3	1	4.3	0	35 40	35 42	19 --	44 --
	22	5	5	2	--	10	30	10	--	--
	23	6	5	2	5.9	10	30	52	--	--
	24	5.5	7.5	--	--	10	30	14	--	--
	25	5	5	2	--	1	30 40	-- --	18 22	-- --
	25					10	30 40	-- --	25 36	-- --
	26	6	5	2	5.9	1	30 40	-- --	10 16	-- --
	30					10	30 40	-- --	20 30	-- --
	27	7.5	3	1	6.6	1	30 40	-- --	13 18	38 48
						10	30 40	-- --	18 27	29 42

35 <sup>2</sup> .5% Na added.<sup>3</sup> Zinc oxide used in preparation.

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Table III (Continued)

## Universal Carbon Formulation Tests

5	Sample #	Impregnants (by wt. percent)					Bed Depth (mm)	Service Life (min)		
		Zn	Cu	Mo	SO <sub>4</sub> <sup>2-</sup>	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
	28	11	--	--	5.9	5	35 40	43 48	19 22	48 57
	29	9	2	1	5.9	5	35 40	55 --	19 23	47 55
	30	7	4	1	5.9	5	35 40	53 --	19 22	47 50
	31	9.5	2	1	5.1	5	35 40	54 --	20 23	42 50
15	32	9.5	2.5	1	5.1	6	35 40	48 51	21 24	43 55
	33	8.5	3	1	3.7	6	35 40	43 48	22 25	50 53
20	34	8.5	3	1	3.7	6	35 40	39 48	23 26	51 58

Formulations containing various loadings of copper and zinc carbonates (as CuCO<sub>3</sub>, ZnCO<sub>3</sub> or equivalents) and copper and zinc as sulfates (as CuSO<sub>4</sub>, ZnSO<sub>4</sub> or equivalents) or copper, zinc and sulfates as well as molybdenum onto granular coal-based 12x30 mesh carbon were discovered to have desirable NH<sub>3</sub>, SO<sub>2</sub>, and CCl<sub>4</sub> breakthrough performances.

Significant moisture loadings on the impregnated materials were discovered to be an important factor in enhancing the performance of the carbons. In some formulations, adequate moisture levels are necessary so that the material may unequivocally meet the CEN specification limits for SO<sub>2</sub> breakthrough performance using desirable lower fill volumes (*i.e.*, < 350 ml). Basic metal carbonates (or oxides) loadings (as CuCO<sub>3</sub> and/or ZnCO<sub>3</sub> equivalents) of greater than 7 wt.% (and with

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moisture loadings of approximately 7%) onto the granular carbons were required to meet SO<sub>2</sub> specification limits at competitive fill volumes. The results of these evaluations are also set forth in Table III.

- 5           In samples including an impregnation of zinc as zinc oxide, no negative effect on the performance of the final material is noted; zinc oxide may therefore be used in place of zinc carbonate.

- One preferred formulation contains the basic  
10 metal carbonates (or oxides) (approximately 8-9 wt.% Zn and/or Cu; as ZnCO<sub>3</sub> and/or CuCO<sub>3</sub>, equivalents) and metal sulfates (2-3 wt.% Zn and/or Cu, as ZnSO<sub>4</sub> and/or CuSO<sub>4</sub>, equivalents) and low levels of molybdenum oxide (approximately 1-3 wt.% Mo (VI), as MoO<sub>3</sub> or MoO<sub>4</sub><sup>2-</sup>,  
15 equivalents), in conjunction with significant moisture loadings (approximately 4-8 wt.%) on the final impregnated carbon. The addition of molybdenum prevents an excessive generation of (CN)<sub>2</sub> when subjecting a copper(II) metal impregnated carbon to the HCN challenge agent, as  
20 excessive levels of (CN)<sub>2</sub> created during the reaction of HCN with a copper(II) species may lead to premature breakthrough of the toxic cyanogen species and an abbreviated service life of the respirator product when subjected to the HCN agent.

- 25           In producing a chromium-free universal A-B-E-K product, all critical constituents should preferably be applied to the substrate using a single impregnation solution; and the resulting mixture could thereafter be, if necessary, thermally processed into the universal  
30 carbon product. In addition to this single impregnation method, a method involving a second impregnation (by solution or spray operation) can also be used to achieve the desired impregnant loadings. This two-step  
35 high-impregnate loadings, or application of a different impregnate than is applied during the first impregnation loading.

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Drying the impregnated material can be achieved by a variety of methods. One desired method includes placing the carbon in a shallow tray in a forced air convection oven. The samples in Table III were prepared by heating at up to 180°C. Higher drying temperatures were observed to be beneficial to performance against ammonia. Tests to determine the effects of these temperatures on the product are set forth in Table IV. Other drying technologies should likewise result in improved ammonia service life, as well as offering other performance and manufacturing benefits.

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Table IV

Effects of Drying Time and Temperature\*

Sample ID	Final Drying Temp.	Bed Depth (mm)	Service Life (min)		
			NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
1A	180°C	35	42	23	48
		40	48	26	54
1B	180°C add. hour	35	43	--	--
		40	55	24	--
2A	195°C	35	47	19	44
		40	51	18	53
2B	210°C	35	51	18	53
		40	58	21	--

\* Wt. % makeup of all formulations: 8.5% Zn, 3.0% Cu, 1.0% Mo, 4.3% SO<sub>4</sub><sup>2-</sup>, 6% H<sub>2</sub>O

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Additional comparative performance studies were conducted using several potential copper and zinc formulations. The results of this optimization study are set forth in Table V. Preparation procedures were similar to those set forth in Table III, except that higher drying temperatures were utilized.

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Table V

## Universal Carbon Optimization Formulation Tests

5	Sample #	Impregnants (by wt. percent)					Bed Depth (mm)	Service Life (min)		
		Zn	Cu	Mo	SO <sub>4</sub> <sup>2-</sup>	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
10	1.	5.5	5.5	1.5	3.5	7	35 40	44 52	22 28	46 --
	2.	7	4	1.5	2.5	5	35 40	37 43	23 26	48 --
	3.	4	7	1.5	4.5	5	35 40	44 52	23 27	45 --
15	4.	7	4	1.5	4.5	5	35 40	48 58	19 22	48 --
	5.	7	4	1.5	2.5	9	35 40	38 46	24 31	47 --
20	6.	5.5	5.5	1.5	3.5	3	35 40	36 43	18 23	53 --
	7.	5.5	5.5	1.5	3.5	7	35 40	44 51	22 26	43 --
	8.	5.5	5.5	1.5	5.5	7	35 40	57 69	22 26	44 --
25	9.	4	7	1.5	2.5	5	35 40	35 42	24 28	49 --
	10.	4	7	1.5	2.5	9	35 40	37 45	25 31	43 --
30	11.	5.5	5.5	1.5	1.5	7	35 40	29 33	23 28	47 --
	12.	2	9	1.5	3.5	7	33 40	44 48	25 29	46 --
	13.	5.5	5.5	1.5	3.5	11	35 40	48 54	25 31	41 --

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Table V (Continued)

## Universal Carbon Formulation Tests

5	Sample #	Impregnants (by wt. percent)					Bed Depth (mm)	Service Life (min)		
		Zn	Cu	Mo	SO <sub>4</sub> <sup>2-</sup>	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
	14.	7	4	1.5	4.5	9	35 40	53 62	22 26	45 --
	15.	9	2	1.5	3.5	7	35 40	46 56	22 25	45 --
10	16.	4	7	1.5	4.5	9	35 40	54 70	29 34	37 --
	17.	5.5	5.5	1.5	3.5	7	35 40	49 54	26 29	43 --
15	18.	11	0	1.5	3.5	7	35 40	42 46	21 25	49 --
	19.	0	11	1.5	3.5	7	35 40	43 52	25 29	47 --
20	20.	5	5	1.5	3.5	7	35 40	50 57	24 29	45 --
	21.	6	6	1.5	3.5	7	35 40	45 54	25 29	43 --
	22.	0	11	1.5	5.5	11	35	66	31	32
	23.	0	11	1.5	5.5	3	35	57	21	48
25	24.	0	11	1.5	1.5	11	35	37	31	40
	25.	0	11	1.5	1.5	3	35	27	22	52
	26.	11	0	1.5	5.5	11	35	56	22	38
	27.	11	0	1.5	5.5	3	35	49	20	48
30	-----									

The effects of the copper-to-zinc metals ratio can be noted from Tables III and V. In samples having a

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constant metal loading, the effects of changing the ratio of copper and zinc can be observed. Comparing a primarily zinc sample with a primarily copper sample, tests show similar performance for carbon tetrachloride, while the  
5 sulfur dioxide performance is approximately 12% better when the primarily copper formulation is used. In some cases, ammonia performance is also improved.

Ammonia service life is strongly affected by the level of sulfate on the product. An increase of 6-7  
10 minutes in service life results from a 1% increase in sulfate (15% of the CEN Requirement of 40 minutes). Sulfate is required, as the presence of copper and/or zinc alone does not provide maximized protection. The addition of 1% moisture also improved performance by approximately  
15 2 minutes; this performance does not appear to be affected by the choice of zinc or copper.

As such, by making slight modifications to the absolute and relative concentration levels of the various species (i.e., carbonates and sulfates) in the  
20 formulation, one can attain a balance and optimize the sorption properties for the various challenge agents. The impregnated activated carbons of the present invention can thus be tailored according to the above-described formulations, using one or a combination of the methods  
25 described, so as to meet the specific desired performance characteristics for any number of industrial and other needs.



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Sources of Sulfate

It was discovered that the particular source of sulfate should not be a factor in the performance of the product. Two sets of formulations were made with identical levels of all impregnants, with the sources of sulfate being zinc sulfate, copper sulfate, ammonium sulfate, or sulfuric acid. The results of these tests are shown in Table VI. No significant differences are noted for the various forms of sulfate.

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Table VI

Effects of the Source of Sulfate on Performance

15	Form of Sulfate	Impregnants (by wt. percent)				Bed Depth (mm)	Service Life (min)		
		Cu	Zn	Mo	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
	Zinc Sulfate	3.0	8.5	1.5	7	35	42	23	48
						40	48	26	55
20	Copper Sulfate	3.0	8.5	1.5	7	35	42	21	49
						40	45	26	--
	Ammonium Sulfate	3.0	8.5	1.5	7	35	42	23	46
						40	47	26	--
25	Ammonium Sulfate	5.5	5.5	1.5	7	35	44	22	46
						40	52	28	--
	Sulfuric Acid	5.5	5.5	1.5	7	35	45	--	50
						40	--	27	--

30 A preferred formulation of the present invention utilizes uses a substrate of 12x30 mesh coal-based activated carbon, impregnated with 11% Copper, 3.5% Sulfate, 2.0% molybdenum and 7% moisture.

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Impregnation recipe for achieving a preferred formulation is as follows:

	<u>Quantity</u>	<u>Material</u>
	290 ml	H <sub>2</sub> O
5	72.9 g	(NH <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>
	226 ml	NH <sub>4</sub> OH
	22.7 g	(NH <sub>4</sub> ) <sub>2</sub> Mo <sub>2</sub> O <sub>7</sub>
	126.8 g	CuCO <sub>3</sub> Cu(OH) <sub>2</sub>
	30.8	(NH <sub>4</sub> ) <sub>2</sub> SO <sub>4</sub>
10	500 g	12 x 30 mesh granular carbon

The performance of this material can be expected to be nearly 20% better than the CEN specifications for NH<sub>3</sub>, SO<sub>2</sub> and CCl<sub>4</sub> at a test bed depth of 35 mm, and 35% better at a 40 mm bed depth. (See Samples 1 and 2, below.) Table VII demonstrates in part the broad effective and useful ranges of the present universal carbons that may prove to be useful in a variety of applications of the present invention.

20

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TABLE VII

Effective Impregnant Range Tests

	<u>Sample</u>	<u>Impregnants (by wt. percent)</u>					<u>Bed Depth (mm)</u>	<u>Service Life (min)</u>		
		<u>Zn</u>	<u>Cu</u>	<u>Mo</u>	<u>SO<sub>4</sub><sup>2-</sup></u>	<u>H<sub>2</sub>O</u>		<u>NH<sub>3</sub></u>	<u>SO<sub>2</sub></u>	<u>CCl<sub>4</sub></u>
25	1.	0	11.0	2.0	3.5	7	35	47	25	49
	2.	0	11.0	2.0	3.5	7	40	54	29	55
	3.	0	15	2	3.5	7	40	52	30	48
30	4.	15	0	2	3.5	7	40	49	23	50
	5.	0	6	10	0	7	40	47	31	62
	6.	0	10	0	6	7	40	59	24	53
	7.	0	11	2	3.5	0	40	45	20	64
	8.	0	10	2	3	15	40	62	40	41

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Use of Different Substrates

Formulations were also made to specifically test the relative advantages and disadvantages of different substrates, as set forth in Table VIII. (The base carbon used in most tests was granular coal-based 12x30 mesh.) The carbons included with these 12x30 mesh carbons were coal-based 12x20 mesh, 1.2 mm coal-based pellets, and 1.2 mm wood-based pellets. At comparable amount of impregnants per volume of carbon, the 12x30 was clearly the superior material. The 12x30 material was 10-15% better in performance than the 12x20 mesh carbon. The smaller mesh size most likely the cause of this difference. Of the pelleted materials, the coal-based material performed much better than wood-based material, based on ammonia and carbon tetrachloride service life tests. The carbon tetrachloride service life of the 1.2 mm coal pellet substrate was comparable to that obtained using the 12x30 carbon. A product based on 1.2 mm coal-based pellets may pass specifications, although a larger fill volume (relative to 12x30 mesh) would likely be needed to achieve performance 20% higher than the specifications. To avoid this situation, a coal-based pellet of smaller diameter than the 1.2 mm coal-based pellet could be used. (Note that the impregnant loadings (on a wt. basis) for Table VIII were changed to compensate for differences in the density of the different carbon substrates.)

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 Table VIII

 Comparison of Various Carbon Substrates  
 (35 mm bed depth)

Sample	Impregnants (by wt. percent)					Substrate	Service Life (min)		
	Zn	Cu	Mo	SO <sub>4</sub> <sup>2-</sup>	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
1.	8.5	3.0	1.0	4.3	6	12x30 mesh	42	23	48
2.	8.5	3.0	1.0	4.3	6	12x20 mesh	39	19	43
3.	10.2	3.6	1.2	5.1	6	1.2mm coal pellets	34	17	46
4.	10.2	3.6	1.2	5.1	6	1.2mm wood pellets	23	17	38

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Comparative performance tests were also run on HCN and (CN)<sub>2</sub> agents using different substrates, to determine the feasibility of using these various substrates as may be desirable in specific applications of the universal product. The performance of these copper/zinc/sulfate/molybdenum formulations are set forth in Table IX below. (Note that the impregnant loadings (on a wt. basis) for Table IX were changed to compensate for differences in the density of the different carbon substrates.)

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Table IX  
Performance Results For Various Substrates

Sample	Impregnants (by wt. percent)					Substrate	Service Life (min)		
	<u>Cu</u> <sup>2</sup>	<u>Zn</u> <sup>3</sup>	<u>Zn</u> <sup>4</sup>	<u>Mo</u> <sup>5</sup>	<u>H<sub>2</sub>O</u>		<u>NH<sub>3</sub></u>	<u>HCN</u>	<u>(CN)<sub>2</sub></u>
1.	5	2	4	2	10	gran.mesh (12x20)	36	33	34
2.	5	2	4	2	10	gran.mesh (12x30)	52	46	45
3.	6	2.4	4.8	2.4	10	1.2mm coal pellets	33	30	31
4.	6	2.4	4.8	2.4	10	1.2mm wood pellets	20	22	24

1 CEN Test Conditions for Class 2 Respirators; Media Bed Depth is 30 mm.

2 Cu added as  $\text{CuCO}_3 \cdot \text{Cu(OH)}_2$

3 Zn added as  $\text{ZnCO}_3$

4 Zn added as  $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$

5 Mo added as  $(\text{NH}_4)_2\text{Mo}_2\text{O}_7$

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### Chloride, Hydrogen Sulfide and Formaldehyde Testing

Testing was also conducted to evaluate the performance of the certain formulations against the other challenge gases ( $\text{Cl}_2$  and  $\text{H}_2\text{S}$ ) defined by the CEN specifications. (See Table X). Studies were also completed on the service life of certain formulations under  $\text{CH}_2\text{O}$  challenge. (See Table XI).

The the  $\text{Cl}_2$  and  $\text{H}_2\text{S}$  challenge tests show that the  $\text{H}_2\text{S}$  performance was more than double the required 40 minutes and the  $\text{Cl}_2$  was 50% above the specification of 20 minutes. During the chlorine testing, the  $\text{HCl}$  concentration was also monitored as the possibility exists for  $\text{Cl}_2$  to be converted to  $\text{HCl}$ . The background level of each was approximately 0.1 ppm (breakthrough = 0.5 ppm  $\text{Cl}_2$ ).

Table X

Testing for  $\text{Cl}_2$  and  $\text{H}_2\text{S}$  Service Life

Sample ID	Impregnants (by wt. percent)					Bed Depth (mm)	Service Life (min)	
	Zn	Cu	Mo	$\text{SO}_4^{2-}$	$\text{H}_2\text{O}$		$\text{H}_2\text{S}$	$\text{Cl}_2$
1	5.5	5.5	1.5	3.5	7	35	92	30
2	0.0	9.7	1.6	3.0	7.5	25	45	16
3	0.0	9.7	1.6	3.0	7.5	35	83	31
4	0.0	9.7	1.6	3.0	7.5	45	----	42

Formaldehyde challenge testing was also performed. The NIOSH Requirement for  $\text{CH}_2\text{O}$  challenge is 50 minutes. The results of these tests are set forth in Table XI. In view of the large difference in formaldehyde performance, it is likely that the presence of sulfate enhances formaldehyde removal, and may make the universal product useful against formaldehyde.

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Table XITesting for CH<sub>2</sub>O Service Life\*

5	<u>Sample No.</u>	<u>Impregnants (by wt. percent)</u>					CH <sub>2</sub> O Break- through (min)
		<u>Zn</u>	<u>Cu</u>	<u>Mo</u>	<u>Cr</u>	<u>SO<sub>4</sub><sup>2-</sup></u>	
	1	0	8	0	3	0	116
	2**	5.5	7.5	0	0	0	38
10	3	5	5	2	0	0	64
	4***	8.5	3	1	0	4.3	>124

- 15 \*
- Cartridges were first equilibrated at 12.5 LPM, 25°C, and 25% RH using NIOSH test procedures; A standard cartridge (93 ml fill) was tested and 32 LPM, 25°C, 25% RH, and 100 ppm CH<sub>2</sub>O.
- \*\* Test sample 12x20 mesh.
- \*\*\* Test terminated without breakthrough.

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Levels of Molybdenum

Tests on the effects of using various levels of molybdenum in the present invention were also conducted, as set forth in Table XII. From this data it can be seen that molybdenum can significantly enhance ammonia service life without affecting adversely the SO<sub>2</sub> or CCl<sub>4</sub> life when the total metal loading remains the same.

Table XII

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## Effects of Molybdenum

		Impregnants (by wt. percent)					Bed Depth (mm)	Service Life (min)		
		Zn	Cu	Mo	SO <sub>4</sub> <sup>2-</sup>	H <sub>2</sub> O		NH <sub>3</sub>	SO <sub>2</sub>	CCl <sub>4</sub>
15	<u>Sample ID</u>									
	1.	12.5	0	0	4.3	6	35	30	22	51
	2.	11.5	0	1	4.3	6	35	38	25	49
	3.	5.5	5.5	1.5	3.5	7	35	45	22	46
	4.	5	5	2.5	3.5	7	35	52	25	--
20	5.	0	11	1.5	4	5	35	47	23	47
	6.	0	10	2.5	4	5	35	64	22	45
	7.	0	11	2.5	4	5	35	55	23	--
	8.	0	11	4.5	0	7	35	40	27	49
	9.	0	0	5	0	7	35	19	13	--

25

As demonstrated in Table XII, the use of molybdenum in the formulation results in significant improvement in NH<sub>3</sub> breakthrough performance. As shown above, and in Table IX, the presence of molybdenum in formulations not including zinc as an impregnate is also essential to maximize performance, particularly under HCN and (CN)<sub>2</sub> challenge.

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Molybdenum has proven to be an important impregnate in the carbons of the present invention, in stabilizing HCN and  $(\text{CN})_2$  performance, and in increasing  $\text{NH}_3$  breakthrough performance across a range of copper and zinc impregnation levels.

Of the various impregnation methodologies, the preferred, and perhaps most reliable, method is the simultaneous impregnation of all necessary constituents using a single impregnation solution. This solution is then utilized in the treatment of an activated carbon substrate. In this method, the impregnation solution must be ammoniacal in order to attain complete dissolution of the basic metal carbonates (or oxides). The use of  $\text{ZnSO}_4$ ,  $\text{CuSO}_4$  and/or basic metal carbonates or oxides,  $\text{ZnCO}_3$ ,  $\text{ZnO}$ ,  $\text{CuCO}_3$  and/or  $\text{CuO}$  can be used to achieve the desired metal loadings. The necessary sulfate levels may be achieved by adding sulfate by a number of different means. Methods of preparation may include one, two or more impregnation cycles by liquid, spray or other application of the selected impregnates.

The activated carbons of the present invention can be tailored according to the described formulations to meet specific desired performance characteristics for any number of industrial and other needs. Although the impregnated carbons offered by the present invention have been described in detail in the foregoing for purposes of illustration, it is to be understood that such details are solely for that purpose and that variations may be made therein by those skilled in the art without departing from the spirit and scope of the invention as described in the following claims.

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WHAT IS CLAIMED:

1. An impregnated activated carbon adsorbent having, by weight, up to 10% sulfate and up to 10% molybdenum and at least one impregnate selected from the group of copper and zinc, said copper being present in an amount of from 0.0 to about 20%, and said zinc is present in an amount of 0.0 to about 20%.

2. An impregnated activated carbon adsorbent as set forth in Claim 1, wherein aqueous ammonia is used as a solvent to dissolve at least one impregnate selected from the group of sulfate, copper, zinc and molybdenum for impregnation on said activated carbon.

3. An impregnated activated carbon adsorbent as set forth in Claim 1, to which up to about 25% H<sub>2</sub>O is added.

4. An impregnated activated carbon adsorbent as set forth in Claim 1, wherein said sulfate is present in an amount from about 2.5 to 4.5%, said copper is present in an amount from about 9 to 13%, said molybdenum is present in an amount from about 1 to 4%, and wherein from about 5 to 10% H<sub>2</sub>O is added to said impregnated activated carbon.

5. An impregnated activated carbon adsorbent as set forth in Claim 4, wherein the unimpregnated activated carbon substrate is of a lower density and the amount of impregnate is increased substantially in proportion to said density in order to provide comparable weight impregnants per volume of substrate.

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6. An impregnated activated carbon adsorbent as set forth in Claim 1, wherein the activated carbon is dried after each impregnation by heating said activated carbon at up to ignition temperature.

7. An impregnated activated carbon adsorbent as set forth in Claim 1, wherein said copper and zinc is impregnated on the activated carbon using at least one solution which contains at least one impregnate selected from the group of copper, copper sulfate, copper carbonate, zinc, zinc sulfate, zinc carbonate and zinc oxide.

8. An impregnated activated carbon adsorbent as set forth in Claim 7, wherein aqueous ammonia is used as a solvent to dissolve said at least one impregnate selected from the group of sulfate, copper, zinc and molybdenum for impregnation on said activated carbon.

9. An impregnated activated carbon adsorbent as set forth in Claim 7, to which up to about 25%  $H_2O$  is added.

10. An impregnated activated carbon adsorbent as set forth in Claim 7, wherein said sulfate is present in an amount from about 2.5 to 4.5%, said copper is present in an amount from about 9 to 13%, said molybdenum is present in an amount from about 1 to 4%, and wherein from about 5 to 10%  $H_2O$ , by weight, is added to said impregnated activated carbon.

11. An impregnated activated carbon adsorbent as set forth in Claim 10, wherein the unimpregnated activated carbon substrate is of a lower density and the amount of impregnate is increased substantially in proportion to said density in order to provide comparable weight of impregnants per volume of substrate.

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12. An impregnated activated carbon adsorbent as set forth in Claim 7, wherein the activated carbon is dried after each impregnation by heating said activated carbon at up to ignition temperature.

13. A method of preparation of an activated carbon adsorbent comprising the steps:

A. preparing a solution containing sulfate and molybdenum and at least one impregnate selected from the group of copper and zinc;

B. impregnating said activated carbon at least once with said solution.

14. A method of preparation of an activated carbon adsorbent as set forth in Claim 13, wherein said sulfate is present in an amount of up to about 10%, said molybdenum is present in an amount of up to about 10%, said copper is present in an amount of from 0.0 to about 20%, and said zinc is present in an amount of from 0.0 to about 20%.

15. A method of preparation of an activated carbon adsorbent as set forth in Claim 13, wherein said sulfate is present in an amount from about 2.5 to 4.5%, said copper is present in an amount from about 9 to 13%, said molybdenum is present in an amount from about 1 to 4%, and wherein from about 5 to 10%  $H_2O$ , by weight, is added to said impregnated activated carbon.

16. A method of preparation of an activated carbon adsorbent as set forth in Claims 13, 14 or 15, further comprising the step:

C. drying the activated carbon after each impregnation prior to the addition of any water.

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17. A method of preparation of an activated carbon adsorbent as set forth in Claims 13 or 14 further comprising the steps:

C. drying the activated carbon after each impregnation by heating said activated carbon at up to ignition temperature; and

D. thereafter impregnating said activated carbon adsorbent with up to 25%  $H_2O$ .

18. A process for removing toxic gases or vapors from a stream utilizing an impregnated activated carbon adsorbent having, by weight, of up to about 10% sulfate and up to 10% molybdenum and at least one impregnate selected from the group of copper and zinc, said copper being present in an amount of from 0.0 to about 20%, said zinc is present in an amount of 0.0 to about 20%.

19. A process as set forth in Claim 18 for removing toxic gases or vapors from a stream utilizing an impregnated activated carbon adsorbent, wherein aqueous ammonia is used as a solvent to dissolve at least one impregnate selected from the group of sulfate, copper, zinc and molybdenum for impregnation on said activated carbon.

20. A process as set forth in Claim 18 for removing toxic gases or vapors from a stream utilizing an impregnated activated carbon adsorbent, wherein said activated carbon adsorbent also contains 0.0 to about 25%  $H_2O$ .

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21. A process as set forth in Claims 18, 19 or 20, wherein said sulfate is present in an amount of about 2.5 - 4.5%, said copper is present in an amount of about 9 - 13%, said molybdenum is present in an amount of about 1 - 4%, and wherein about 5 - 10%  $H_2O$  is added to said impregnated activated carbon.

22. A process as set forth in Claim 18 for removing toxic gases or vapors from a stream utilizing an impregnated activated carbon adsorbent, wherein the activated carbon is dried after each impregnation by heating said activated carbon at up to ignition temperature.

23. A process as set forth in Claim 18 for removing toxic gases or vapors from a stream utilizing an impregnated activated carbon adsorbent, wherein said copper and zinc is impregnated on the activated carbon using at least one solution which contains at least one impregnate selected from the group of copper, copper sulfate, copper carbonate, zinc, zinc sulfate, zinc carbonate and zinc oxide.

24. A method useful in industrial applications for removing toxic gases or vapors including chlorine, hydrogen chloride, hydrogen cyanide, sulfur dioxide, hydrogen sulfide, formaldehyde, ammonia, mercaptans, bromine, hydrogen fluoride, hydrogen bromide, methylamine and other amines, phosgene, organic vapors such as carbon tetrachloride and others, utilizing a protective filter or respirator containing an impregnated activated carbon adsorbent having, by weight, up to about 10% sulfate and up to 10% molybdenum and at least one impregnate selected from the group of copper and zinc, said copper being present in an amount of from 0.0 to about 20% and said zinc is present in an amount of 0.0 to about 20%.

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25. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 24, wherein aqueous ammonia is used as a solvent to dissolve at least one impregnate selected from the group of sulfate, copper, zinc and molybdenum for impregnation on said activated carbon.

26. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 24, to which up to about 25%  $H_2O$  is added to the impregnated activated carbon.

27. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 24, wherein said sulfate is present in an amount from about 2.5 to 4.5%, said copper is present in an amount from about 9 to 13%, said molybdenum is present in an amount from about 1 to 4%, and wherein from about 5 to 10%  $H_2O$ , by weight, is added to said impregnated activated carbon.

28. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 24, wherein said unimpregnated activated carbon substrate is of a lower density and the amount of impregnate is increased substantially in proportion to said density in order to provide comparable weight impregnants per volume of substrate.

29. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 24, wherein the activated carbon is dried after each impregnation by heating said activated carbon at up to ignition temperature.

30. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 24, wherein said copper and zinc is impregnated on the activated carbon using at least one solution which contains at least one impregnate selected from the group of copper, copper sulfate, copper carbonate, zinc, zinc sulfate, zinc carbonate and zinc oxide.

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31. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 30, wherein aqueous ammonia is used as a solvent to dissolve at least one impregnate selected from the group of sulfate, copper, zinc and molybdenum for impregnation on said activated carbon.

32. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 30, to which up to about 25% H<sub>2</sub>O is added to the impregnated activated carbon.

33. A method useful in industrial applications of removing toxic gases or vapors as set forth in Claim 30, wherein said sulfate is present in an amount from about 2.5 to 4.5%, said copper is present in an amount from about 9 to 13%, said molybdenum is present in an amount from about 1 to 4%, and wherein from about 5 to 10% H<sub>2</sub>O, by weight, is added to said impregnated activated carbon.

34. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 30, wherein said impregnated carbon substrate is of a lower density and the amount of impregnate is increased substantially in proportion to said density in order to provide comparable weight impregnants per volume of substrate.

35. A method useful in industrial applications for removing toxic gases or vapors as set forth in Claim 30, wherein the activated carbon is dried after each impregnation by heating said activated carbon at up to ignition temperature.



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36. A filter for removing toxic gases comprising an activated carbon absorbent impregnated with up to 10% sulfate and up to 10% molybdenum and at least one impregnate selected from the group consisting of copper and zinc where said copper is present in an amount from 0.0 to about 20% and zinc is present in an amount from 0.0 to about 20% wherein said percentages are by weight.

37. A filter as set forth in Claim 36 including up to 25% H<sub>2</sub>O added to said impregnated activated absorbent.

38. A respirator for protection against Types A, B, E and K toxic agents and others, said respirator including a filter as set forth in Claim 36 or 37.

39. A respirator for protection against agents including chlorine, hydrogen chloride, hydrogen cyanide, sulfur dioxide, hydrogen sulfide, formaldehyde, ammonia, mercaptans, bromine, hydrogen fluoride, hydrogen bromide, methylamine and other amines, phosgene, organic vapors such as carbon tetrachloride and others, said respirator including a filter as set forth in Claim 36 or 37.

40. A universal filter as set forth in Claim 36 wherein said copper is added in the form of one of copper, copper sulfate or copper carbonate, and zinc is added in the form of one of zinc, zinc sulfate, zinc carbonate or zinc oxide.

41. A respirator including a filter as set forth in Claim 36 or 37.

42. A universal filter for the removal of Types A, B, E and K toxic gases comprising an activated carbon adsorbent impregnated with about 2.5 to 4.5% sulfate, about 9 to 13% copper, about 1 to 4% molybdenum and containing 5 to 10% H<sub>2</sub>O.

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43. A universal filter as set forth in Claim 42 wherein said copper is added in the form of one of copper, copper sulfate or copper carbonate and zinc is added in the form of one of zinc, zinc sulfate, zinc carbonate or zinc oxide.

44. A respirator including a filter as set forth in Claim 42.

## INTERNATIONAL SEARCH REPORT

PCT/US92/10216

**A. CLASSIFICATION OF SUBJECT MATTER**

IPC(5) : B01J 20/20; C01B 17/16; C01C 1/12, 3/04; B01D 53/34; A62B 23/00

US CL : 502/417, 416, 183; 423/230, 236, 237, 241, 244.03, 245.1

According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 502/417, 416, 183; 423/230, 236, 237, 241, 244.03, 245.1

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US, A, 4,677,096 (VAN DER SMISSEN) 30 June 1987. See col. 3 and 4.	1-35
X	US, A, 2,920,051 (WIIG ET AL.) 05 January 1960. See col. 2, and col. 4, lines 32-34.	1-35
X	US, A, 3,355,317 (KEITH II, ET AL.) 28 November 1967. See col. 2, and claim 4.	1-35
Y	DD, A, 237,154 A1 (BILLIG ET AL) 07 February 1986. See Abstract.	1, 3,6, 7, 12, 14, 16, 18-20, 24, 26, 28-30, 32, 34, 35

☒ Further documents are listed in the continuation of Box C.
 ☐ See patent family annex.

* Special categories of cited documents:	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"A" document defining the general state of the art which is not considered to be part of particular relevance	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"E" earlier document published on or after the international filing date	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"I" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"Z" document member of the same patent family
"O" document referring to an oral disclosure, use, exhibition or other means	
"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search

11 FEBRUARY 1993

Date of mailing of the international search report

03 MAR 1993

 Name and mailing address of the ISA/US  
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## INTERNATIONAL SEARCH REPORT

International application No.

PCT/US92/10216

**Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)**

This international report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:  
because they relate to subject matter not required to be searched by this Authority, namely:
2. ☐ Claims Nos.:  
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:
3. ☐ Claims Nos.:  
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

**Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)**

This International Searching Authority found multiple inventions in this international application, as follows:

I. Claims 1-35 drawn to an impregnated activated carbon, the method of preparing said carbon and the use of said carbon, classified in Class 502, subclass 417.

II. Claims 36-44 drawn to a filter apparatus - respirator classified in Class 128, subclass 200.24.

1. ☐ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2. ☐ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3. ☐ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:
4. ☒ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:  
1-35

Remark on Protest

☐

The additional search fees were accompanied by the applicant's protest.

☐

No protest accompanied the payment of additional search fees.

## INTERNATIONAL SEARCH REPORT

International application No.  
PCT/US92/10216

## C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X,P	US, A, 5,113,856 (VAN DER SMISSEN) 19 May 1992. See col. 1 and 2.	1-35
A	US, A, 4,801,311 (TOLLES) 31 January 1989. See the entire document.	1-35